



# Facile one-pot synthesis of Fe-UZM-35 catalysts for ammonia selective catalytic reduction

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## ABSTRACT

Owing to the narrow crystallization field, the synthesis of the large-pore zeolite UZM-35 with MSE topology starting from amorphous reagents in the presence of dimethyldipropylammonium ions as an organic structure-directing agent is often non-reproducible. Here we report the synthesis of UZM-35 via an interzeolite conversion route using USY zeolites, as the sole source of Al and Si, and a small amount of previously synthesized UZM-35 as seed crystals. We also present the one-pot synthesis of Fe-UZM-35 with the best low-temperature NH<sub>3</sub>-SCR activity among the iron-exchanged zeolites reported so far. These synthesis routes showed high reproducibility, together with considerably faster crystallization kinetics ( $\leq 1.5$  vs 7 days) compared to conventional UZM-35 synthesis. When the Fe loading level was properly adjusted, the NH<sub>3</sub>-SCR activity of one-pot-synthesized Fe-UZM-35 was found to be essentially the same as that of post-synthetically exchanged Fe-UZM-35 due to the similarity in the nature of their iron active sites.

## 1. Introduction

Despite an ambitious global market ramp-up of battery-electric passenger vehicles over the past decade, it is likely that diesel vehicles with high NO<sub>x</sub> (NO and NO<sub>2</sub>) emissions will not be completely phased out from our daily lives in the near future. In fact, diesel heavy-duty vehicles are predicted to remain a major freight transportation sector and should not be replaced by electric ones even in California at least until 2040, not only because of the economic reason but also because of the overall emission control strategy [1]. This becomes clearer when considering common rail systems, long-distance ships, and heavy construction and agriculture equipment, which currently use diesel engines, but might be difficult to be ubiquitously electrified before long.

Among the diesel exhaust after-treatment technologies developed so far, selective catalytic reduction of NO<sub>x</sub> by NH<sub>3</sub> (NH<sub>3</sub>-SCR) is most successful, but presents many challenges [2–4]. For example, the current commercial copper-exchanged SZZ-13 (framework type CHA) and SSZ-39 (AEI) catalysts [5,6] have poor resistance to poisoning from residual sulfur in diesel exhaust and favor the formation of N<sub>2</sub>O, another potent greenhouse gas [7], during NH<sub>3</sub>-SCR. In contrast, the other commercial NH<sub>3</sub>-SCR catalysts, iron-exchanged beta and ZSM-5 (MFI) zeolites, with high resistance to sulfur poisoning and N<sub>2</sub>O formation [8,9],

suffer from poor low-temperature (<350 °C) SCR activity. In this respect, Fe-UZM-35 (MSE) with intersecting 12- and 10-ring channels is of special interest, because its low-temperature activity is best among the Fe-zeolites known to date [10,11]. Owing to its lower oxidation state, on the other hand, the Fe<sup>2+</sup> ion can be more favorably exchanged into the aluminosilicate zeolite support than the Fe<sup>3+</sup> ion. However, Fe<sup>2+</sup> exchange in zeolites requires the prevention of Fe<sup>2+</sup> oxidation to trivalent iron species such as FeO(OH), which cannot be easily introduced into the zeolite pores during ion exchange [9,12], requiring the use of inert N<sub>2</sub> atmosphere. One way to overcome such a limitation is the one-pot synthesis of Fe-zeolites (Fig. 1). Compared to Cu-zeolites, nevertheless, less attention to their one-pot synthesis has been paid so far [13–20]. To our knowledge, in particular, no attempt to one-pot-synthesize Fe-UZM-35 have been made yet.

We have previously shown that the Si/Al and K<sup>+</sup>/(Na<sup>+</sup> + K<sup>+</sup>) ratios in the synthesis mixture yielding pure UZM-35 in the presence of dimethyldipropylammonium (DMDPA) ions as an organic structure-directing agent (OSDA) is very narrow [21]. Furthermore, the phase purity of this large-pore zeolite was found to be highly sensitive to crystallization time, giving limited reproducibility to its conventional hydrothermal synthesis starting from amorphous reagents. The interzeolite conversion (IZC) route, pioneered by Zones in the late 1980s

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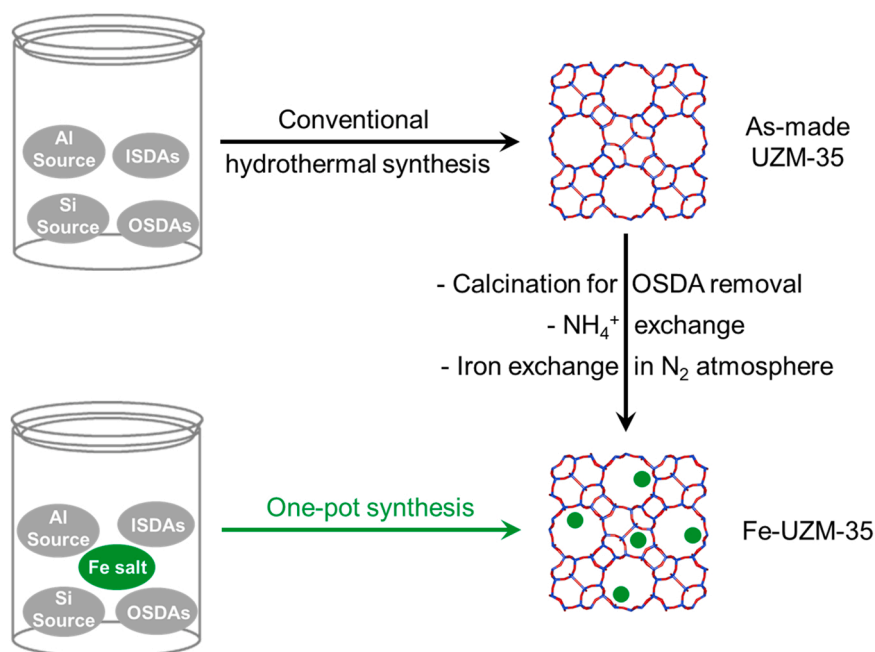


Fig. 1. Schematic illustrations of conventional and one-pot synthesis routes to Fe-UZM-35.

[22–24], includes the use of a particular zeolite as the source of Al, Si, and/or both, most likely zeolite Y (FAU), in the presence or absence of OSDAs. While the number of zeolite structures which can be synthesized through IZC is steadily growing [25], the reproducibility of zeolite synthesis is often method-specific. This has led us to consider whether the IZC route is applicable to the synthesis of UZM-35. Here we show that while the IZC of ultra-stable Y (USY; FAU) zeolites with DMDPA is a highly reproducible route to UZM-35, the one-pot synthesis of Fe-UZM-35 can also be achieved in a similar manner. The overall  $\text{NH}_3$ -SCR activity of one-pot-synthesized Fe-UZM-35 with an Fe/Al ratio of 0.23 (2.3 Fe wt%) was found to be comparable with that of post-synthetically exchanged Fe-UZM-35 with essentially the same Fe/Al ratio (0.24).

## 2. Experimental

### 2.1. Zeolite synthesis

The reagents used in this study included DMDPAOH (40%, Sachem), NaOH (50% aqueous solution, Aldrich), KOH (45% aqueous solution, Aldrich), aluminum hydroxide ( $\text{Al}(\text{OH})_3 \cdot 1.0 \text{ H}_2\text{O}$ , Aldrich), colloidal silica (Ludox HS-40, Dupont), three USY zeolites with Si/Al ratios of 7.5 (HSZ-360-HUA, Tosoh), 15 (CBV720, Zeolyst), and 30 (CBV760, Zeolyst),  $\text{FeSO}_4 \cdot 7 \text{ H}_2\text{O}$  (99%, Aldrich),  $\text{CuSO}_4 \cdot 5 \text{ H}_2\text{O}$  (98%, Aldrich), and  $\text{NH}_4\text{NO}_3$  (98.5%, Alfa).

The conventional hydrothermal synthesis of UZM-35, which uses  $\text{Al}(\text{OH})_3 \cdot 1.0 \text{ H}_2\text{O}$  and Ludox HS-40 as Al and Si sources, respectively, was carried out according to the procedures given elsewhere [21]. Its IZC synthesis that uses USY as the sole source of Al and Si, as well as the one-pot synthesis of Fe-UZM-35, was performed using aluminosilicate gels with the composition  $4.50\text{DMDPAOH} \cdot 0.25\text{Na}_2\text{O} \cdot 0.75 \text{ K}_2\text{O} \cdot x\text{Fe}^{\text{II}}\text{O} \cdot y\text{Al}_2\text{O}_3 \cdot 10.0\text{SiO}_2 \cdot 155 \text{ H}_2\text{O}$ , where  $x$  and  $y$  are varied between  $0 \leq x \leq 0.50$  and  $0.017 \leq y \leq 0.067$ , respectively. If required, a small amount of previously synthesized and calcined UZM-35 (4 wt% of USY used) was added as seed crystals. The one-pot synthesis of Cu-UZM-35 was also attempted in a similar manner to that of Fe-UZM-35. After being stirred for 2 h at a room temperature, the final mixture was placed into a 45 mL Teflon-lined autoclave and heated under static conditions at  $170^\circ\text{C}$  for 0.5–7 days. The solid products were recovered by centrifugation, washed repeatedly

with deionized water, and dried overnight at room temperature. As-made Fe-UZM-35 and Cu-UZM-35 were refluxed twice in 1.0 M  $\text{NH}_4\text{NO}_3$  solutions (1 g solid per 100 mL solution) for 6 h and then calcined in air at  $550^\circ\text{C}$  for 8 h, prior to their use as catalysts for  $\text{NH}_3$ -SCR.

Fe-UZM-35 and Cu-UZM-35 were also prepared by iron exchange of the ammonium form of UZM-35 synthesized by the conventional method, following the procedures described in our previous work [10, 11, 21]. All catalysts prepared here were hydrothermally aged at  $750^\circ\text{C}$  in air for 12 h, using flowing air consisting of 10%  $\text{H}_2\text{O}$ . While the UZM-35 zeolites synthesized via conventional and IZC synthesis routes were referred to as UZM-35(C) and UZM-35(IZC), respectively, the Fe-UZM-35 zeolites obtained by iron exchange of  $\text{NH}_4$ -UZM-35(C) and one-pot synthesis were denoted as Fe-UZM-35(C) and Fe-UZM-35(OP), respectively. When necessary, in addition, their Fe/Al ratio was attached to the catalyst name. For comparison, Fe-beta with Fe/Al = 0.21 was prepared by iron exchange of  $\text{NH}_4$ -beta with Si/Al = 12.5 (CBV814E, Zeolyst) and designated in a manner similar to that given above.

### 2.2. Catalysis

$\text{NH}_3$ -SCR was performed in a continuous fixed-bed flow reactor. Before each catalytic run, 0.6 g of catalyst (20/30 mesh) was packed into a 3/8-in.-od aluminum tube reactor and pretreated at  $500^\circ\text{C}$  for 2 h under air flow ( $2000 \text{ mL min}^{-1}$ ). A reactant feed containing NO 500 ppm,  $\text{NH}_3$  500 ppm, 5%  $\text{O}_2$ , and 10%  $\text{H}_2\text{O}$ , balanced with  $\text{N}_2$ , was supplied, and the steady-state SCR conversion was measured at temperature ranging from  $150^\circ$  to  $600^\circ\text{C}$  at a gas hourly space velocity (GHSV) of  $100,000 \text{ h}^{-1}$ . The inlet and outlet gas concentrations were analyzed online by a Thermo Nicolet 6700 FT-IR spectrometer. The apparent activation energy ( $E_{\text{app}}$ ) was determined from the slope of the Arrhenius plot according to the procedures given in our recent work [11].

### 2.3. Characterization

Powder X-ray diffraction (PXRD) patterns were collected on a PANalytical X'Pert diffractometer with  $\text{Cu K}\alpha$  radiation ( $\lambda = 1.5406 \text{ \AA}$ ). The crystallinity of a series of solid products isolated as a function of

**Table 1**  
Representative synthesis conditions<sup>a</sup> and results.

Run no.	Al source <sup>b</sup>	Si source <sup>b</sup>	Synthesis mixture composition <sup>a</sup>			Product <sup>c</sup>
			x	Si/Al	Fe/Al	
1 <sup>d</sup>	AH	LH	0	10		UZM-35
2 <sup>d</sup>	HSZ-360-HUA		0	7.5		Amorphous
3 <sup>e</sup>	HSZ-360-HUA		0	7.5		Offretite + UZM-35
4 <sup>e</sup>	CBV720		0	15		Amorphous + (UZM-35)
5 <sup>e</sup>	CBV720		0	15		UZM-35
6 <sup>e</sup>	CBV760		0	30		Amorphous + (UZM-35)
7 <sup>e</sup>	CBV760		0	30		UZM-35
8 <sup>e</sup>	CBV760		0.06	30	3.8	Fe-UZM-35
9 <sup>e</sup>	CBV760		0.13	30	7.5	Fe-UZM-35
10 <sup>e</sup>	CBV760		0.25	30	15	Fe-UZM-35
11 <sup>e</sup>	CBV760		0.50	30	30	Amorphous + Fe-UZM-35
12 <sup>e,f</sup>	CBV760		0.06	30	3.8 <sup>g</sup>	Cu-UZM-35
13 <sup>e,f</sup>	CBV760		0.08	30	5.0 <sup>g</sup>	Cu-UZM-35
14 <sup>e,f</sup>	CBV760		0.13	30	7.5 <sup>g</sup>	Cu-UZM-35 + amorphous + (Cu-offretite)

<sup>a</sup> The synthesis mixture composition is 4.50DMDPAOH-0.25Na<sub>2</sub>O-0.75 K<sub>2</sub>O·xFe<sup>III</sup>O·yAl<sub>2</sub>O<sub>3</sub>·10.0SiO<sub>2</sub>·155 H<sub>2</sub>O, where x and y are varied between 0 ≤ x ≤ 0.50 and 0.017 ≤ y ≤ 0.067, respectively. All syntheses were conducted under static conditions at 170 °C for 4 days, unless otherwise stated.

<sup>b</sup> AH, Al(OH)<sub>3</sub>·1.0 H<sub>2</sub>O; LH, Ludox HS-40; HSZ-360-HUA, Tosoh USY with Si/Al = 7.5; CBV720, Zeolyst USY with Si/Al = 15; CBV760, Zeolyst USY with Si/Al = 30.

<sup>c</sup> The product appearing first is the major phase, and the product obtained in a trace amount is given in parentheses.

<sup>d</sup> Obtained after 7 days of heating at 170 °C.

<sup>e</sup> A small amount of calcined UZM-35(C) (4 wt% of USY used as both Si and Al sources) were added as seed crystals.

<sup>f</sup> CuSO<sub>4</sub>·5H<sub>2</sub>O was added instead of FeSO<sub>4</sub>·7H<sub>2</sub>O.

<sup>g</sup> Cu/Al ratio.

crystallization time during the synthesis of UZM-35(IZC) and Fe-UZM-35(OP) under static conditions at 170 °C was determined by comparing the area of the X-ray peak around 2θ = 21.7°, corresponding to the (420) reflection of the MSE structure, with that of as-made UZM-35(C) [26]. The crystallinity of the USY source during their crystallization was estimated by comparing the area of the intense X-ray peak around 2θ = 6.2° assigned to the (111) reflection of the FAU structure with that of CBV760 USY. Crystal morphology and size were identified by a JEOL JSM-6510 scanning electron microscope (SEM). Thermogravimetric analysis (TGA) was conducted on a SII EXSTAR 6000 thermal analyzer, and the weight loss due to the combustion of OSDAs were determined from differential thermal analysis (DTA) using the same analyzer. Elemental analysis was carried out by the Pohang Institute of Metal Industry Advancement. The N<sub>2</sub> adsorption data were obtained on a Mirae SI nanoPorosity-XG analyzer.

<sup>27</sup>Al MAS NMR spectra were measured on a Bruker DRX500 spectrometer at a <sup>27</sup>Al frequency of 130.351 MHz with a π/6 rad pulse length 1.0 μs, a recycle delay of 2.0 s, and an acquisition of ca. 1000 pulse transients. To accurately compare the signal intensity of fresh and hydrothermally aged catalysts, the same amount of sample was used in each experiment. IR spectra in the OH region were taken on a Thermo-Nicolet 6700 FT-IR spectrometer using self-supporting catalyst wafers of ca. 13 mg. Prior to the experiments, the wafer was treated under vacuum (10<sup>-4</sup> Pa) at 450 °C for 2 h inside a home-built IR cell with CaF<sub>2</sub> windows. In situ diffuse reflectance infrared Fourier-transform (DRIFT) spectra were collected on an identical FT-IR spectrometer but with a DRIFT cell (Pike). Before each experiment, about 15 mg of catalyst was heated under air flow (100 mL min<sup>-1</sup>) at 350 °C for 2 h. After being cooled down to 150 °C, a background spectrum was obtained. Then, the catalyst was exposed to 500 ppm NO with 5% O<sub>2</sub> in He for 1 h and then purged in a He flow at the same temperature for another 0.5 h. The spectra were measured and analyzed after subtracting the background.

**Table 2**  
Physical properties of the representative catalysts studied in this work.

Run no. <sup>a</sup>	Catalyst ID	Si/Al <sup>b</sup>	Fe wt % <sup>b</sup>	Fe/Al <sup>b</sup>	Crystal shape and average size <sup>c</sup> (μm)	BET surface area <sup>d</sup> (m <sup>2</sup> g <sup>-1</sup> )
1	UZM-35 (C)	9			Rectangular plates, 0.3 × 0.15	420 (0.18)
5	UZM-35 (IZC)A	7				460 (0.19)
7	UZM-35 (IZC)B	8			Rectangular plates, 3.0 × 1.0	450 (0.19)
8	Fe-UZM-35(OP) 0.13	8	1.3	0.13		440 (0.19)
9	Fe-UZM-35(OP) 0.23	8	2.3	0.23	Rectangular plates, 1.5 × 1.5	440 (0.19)
10	Fe-UZM-35(OP) 0.38	8	3.7	0.38		440 (0.19)
13	Cu-UZM-35(OP) 0.11	7	1.3 <sup>e</sup>	0.11 <sup>f</sup>	Rectangular plates, 1.5 × 1.5	430 (0.19)

<sup>a</sup> The same as those in Table 1.

<sup>b</sup> Determined by elemental analysis.

<sup>c</sup> Determined by SEM.

<sup>d</sup> Determined by N<sub>2</sub> adsorption data of their proton form. The values in parentheses are the micropore volumes in cm<sup>3</sup> g<sup>-1</sup>.

<sup>e</sup> Cu wt%.

<sup>f</sup> Cu/Al ratio.

UV-Vis spectra were taken on a Shimadzu UV-2501PC spectrometer using BaSO<sub>4</sub> as a reference.

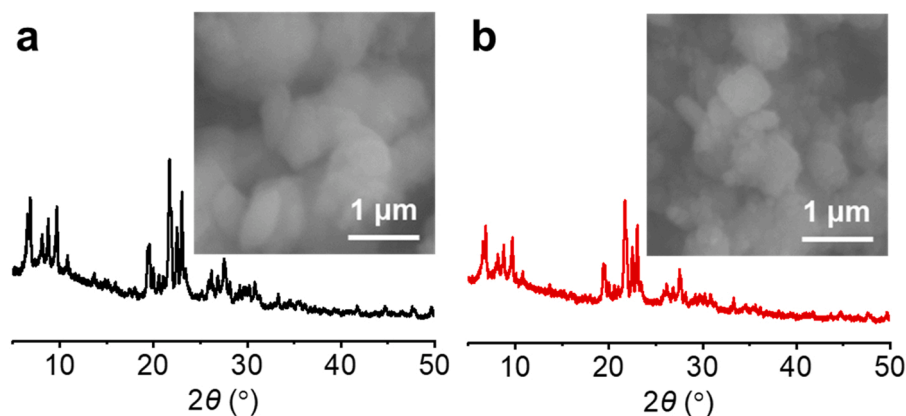
X-band EPR spectra at −148 °C were measured on a Bruker A200 spectrometer with 100 kHz field modulation and 41 s sweep time. The packing height of powdered sample in the tube was kept constant, with its center placed in the middle of the EPR cavity, in order to quantitatively measure the signal intensity. The g value was calibrated with 2,2-diphenyl-1-picrylhydrazyl powder (g = 2.0036). NH<sub>3</sub> temperature-programmed desorption (TPD) was collected on a Hewlett-Packard 5890 series II gas chromatograph with a thermal conductivity detector, as described in our previous paper [27]. The X-ray absorption near edge structure (XANES) spectra at the Cu K-edge were recorded on the 8 C beamline at the Pohang Accelerator Laboratory using a Si (111) crystal monochromator, and further details can be found elsewhere [21].

### 3. Results and discussion

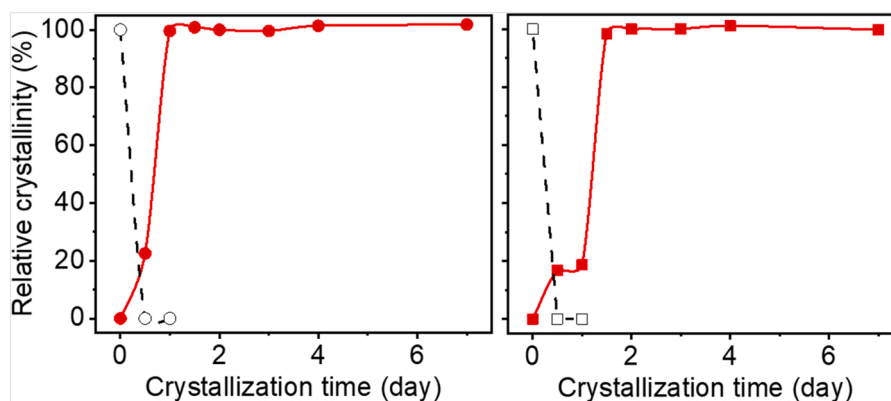
#### 3.1. One-pot synthesis of Fe-UZM-35

Table 1 lists the summary of the IZC synthesis of UZM-35 under static conditions at 170 °C. The products listed in each synthesis run were the only ones found in repeated trials. Our initial attempt to obtain UZM-35 through IZC, with DMPDA as an OSDA, was by replacement of silica in the reported gel composition 4.50DMDPAOH-0.25Na<sub>2</sub>O-0.75 K<sub>2</sub>O-0.5Al<sub>2</sub>O<sub>3</sub>·10.0SiO<sub>2</sub>·150 H<sub>2</sub>O [21] with the equimolar amount of a Tosoh USY (Si/Al = 7.5, HSZ-360-HUA), without adding any Al source. However, the synthesis mixture remained an amorphous phase even after heating at 170 °C for 7 days. This led us to change the USY source to USYs with higher Si/Al ratios of 15 and 30 (i.e., Zeolyst CBV720 and CBV760, respectively) and detect UZM-35 only as a trace phase after 4 days of heating. To facilitate UZM-35 crystallization, therefore, we added a small amount (4 wt% relative to the amount of USY used as a Si source) of calcined UZM-35(C) as seed crystals to the synthesis mixture and carried out the synthesis for the same period of time. As shown in Table 1, we were then able to obtain pure UZM-35 in a highly reproducible manner.

Table 1 also lists the summary of the one-pot synthesis of Fe-UZM-35 performed in this study. The elemental analysis in Table 2 indicates that the Si/Al ratio (8) of UZM-35(IZC) from synthesis run 7 is slightly higher



**Fig. 2.** PXRD patterns and SEM images of as-made (a) UZM-35(IZC) and (b) Fe-UZM-35(OP) obtained from synthesis runs 7 and 9 in Table 1, respectively.



**Fig. 3.** Crystallinities of a series of solid products isolated as a function of time during the synthesis of UZM-35(IZC) (left) and Fe-UZM-35(OP) (right) using the same gels as those of synthesis runs 7 and 9 in Table 1 under static conditions at 170 °C, respectively. Open symbols indicate the crystallinity decrease of the CBV760 USY source.

than that (7) from synthesis run 5. Therefore, various amounts of ferric sulfate were added as an Fe source to the gel used to produce the former material and subject to crystallization at 170 °C, because the hydrothermal stability of metal-exchanged zeolites for  $\text{NH}_3$ -SCR becomes higher with increasing zeolite Si/Al ratio [2]. When the Fe/Al ratio in the synthesis mixture was 15 or lower, pure Fe-UZM-35 was obtained after 4 days of heating. However, we were not able to fully crystallize Fe-UZM-35 from the synthesis mixture with a higher Fe content (e.g., Fe/Al = 30). It is worth noting that while the use of cupric sulfate instead of ferric sulfate under the above synthesis conditions gave Cu-UZM-35, the Cu/Al ratio range (0–5) yielding its pure phase is significantly lower than the Fe/Al ratio range (0–15) for Fe-UZM-35 formation. As a spectator, therefore, the  $\text{Fe}^{2+}$  ion appears to disturb UZM-35 crystallization than the  $\text{Cu}^{2+}$  ion.

The PXRD patterns of as-made UZM-35(IZC) zeolites synthesized here reveal that they are highly crystalline (Fig. 2), as supported by the micropore volumes of their proton forms (Table 2). In particular, there are no reflections from other crystalline phases, which is also the case for as-made Fe-UZM-35(OP) and Cu-UZM-35(OP) zeolites with different Fe/Al (or Cu/Al) ratios (Supplementary Fig. S1). Thus, if any iron or copper oxide species were generated during the one-pot synthesis, their size may not be large enough to be detectable by PXRD. The  $^{27}\text{Al}$  MAS NMR spectra of as-made UZM-35(IZC) and Fe-UZM-35(OP) are characterized by only one resonance around 55 ppm (Supplementary Fig. S2), typical of tetrahedral Al in the zeolite framework. Given that their Si/Al ratio (8) are considerably lower than the ratio (30) of the USY source, a major amount of silica from USY during IZC remains in solution, explaining the low product yield (ca. 25%) of IZC-synthesized UZM-35

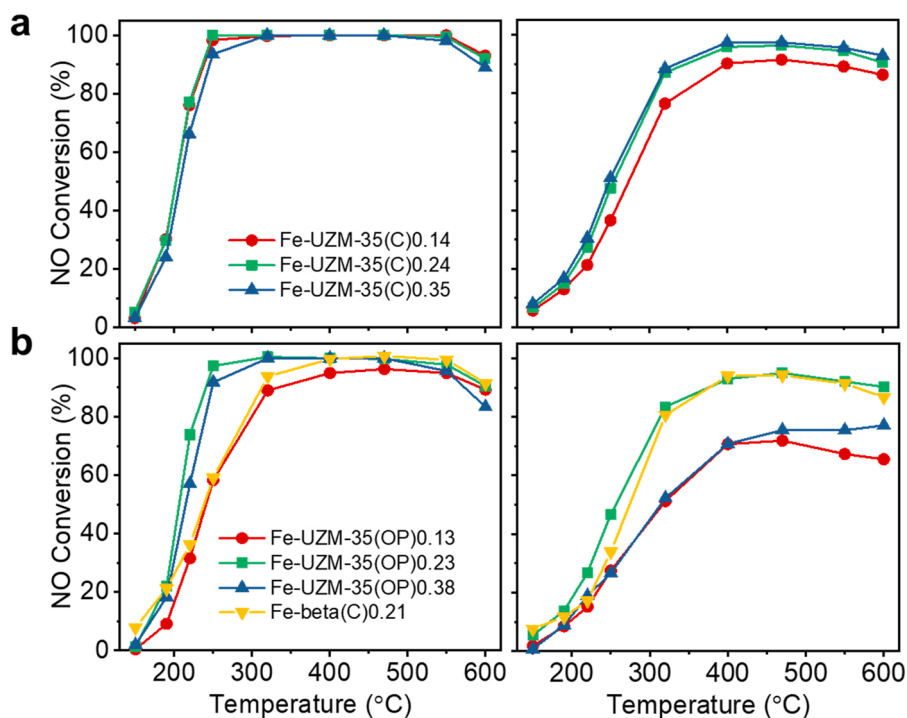
and one-pot-synthesized Fe-UZM-35. We also note that as-made UZM-35 (IZC) and Fe-UZM-35(OP) show similar OSDA contents (Supplementary Fig. S3) and morphologies (Fig. 2) to each other, although their plate-like crystals are less faceted than UZM-35(C) crystals [21].

Fig. 3 shows the crystallization kinetics under static conditions at 170 °C of UZM-35(IZC) and Fe-UZM-35(OP) from gel compositions used for synthesis runs 7 and 9 in Table 1, respectively. It can be seen that their synthesis is almost complete after 1.0 and 1.5 days of heating, respectively. These crystallization times are quite shorter than the UZM-35(C) crystallization time (7 days), most likely because of the UZM-35 (C) seed crystals added. Notably, the retarding effect of  $\text{Fe}^{2+}$  spectator ions on UZM-35 formation is not strong. The fact that all characteristic X-ray peaks from USY entirely disappear within the first 12 h of the synthesis (Supplementary Fig. S4) suggests the dissolution of CBV760 USY crystals in the early stages, prior to UZM-35 formation.

### 3.2. $\text{NH}_3$ -SCR

Fig. 4 shows the NO conversion as a function of reaction temperature over three pairs of Fe-UZM-35(C) and Fe-UZM-35(OP) catalysts with the same zeolite Si/Al ratio (9 or 8) but different Fe/Al ratios (0.13–0.38) in the fresh and 750 °C-aged forms under standard SCR conditions, with 10%  $\text{H}_2\text{O}$  present in the feed. All fresh Fe-UZM-35(C) catalysts exhibited quite similar SCR activities to one another in the reaction temperature region studied (150–600 °C), regardless of the Fe/Al ratio. The same trend could be observed for their 750 °C-aged form, although the low-temperature (<350 °C) NO conversion was rather lower than that of the corresponding fresh UZM-35(C) catalysts [21]. As shown in Fig. 4,



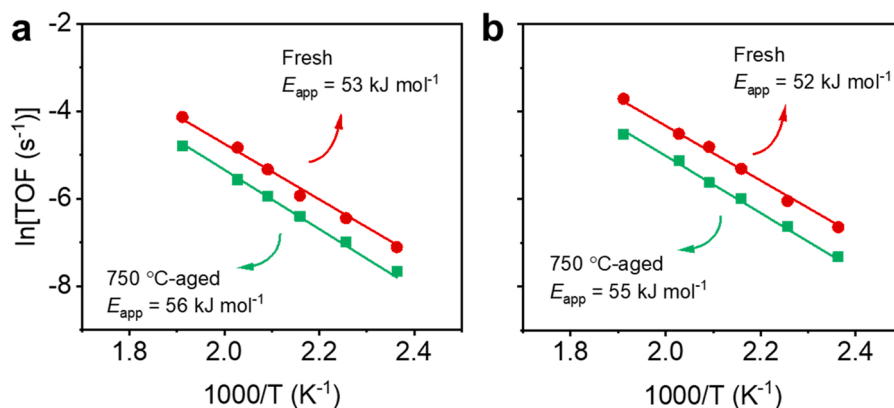


**Fig. 4.** NO conversion as a function of reaction temperature over the fresh (left) and 750 °C-aged (right) forms of (a) Fe-UZM-35(C) and (b) Fe-UZM-35(OP) with different Fe/Al ratios and Fe-beta(C)0.21. The feed contains 500 ppm  $\text{NH}_3$ , 500 ppm NO, 5%  $\text{O}_2$  and 10%  $\text{H}_2\text{O}$  balanced with  $\text{N}_2$  at 100,000  $\text{h}^{-1}$  GHSV. Hydrothermal aging was carried out under flowing air containing 10%  $\text{H}_2\text{O}$  at 750 °C for 12 h.

however, there are notable differences in the  $\text{NH}_3$ -SCR activity of Fe-UZM-35(OP) catalysts, depending on the Fe/Al ratio. For example, the NO conversion over fresh catalysts at 250 °C was higher in the order Fe-UZM-35(OP)0.13 < Fe-UZM-35(OP)0.38  $\approx$  Fe-UZM-35(OP)0.23. In addition, the NO conversion over 750 °C-aged catalysts at the same reaction temperature increased in the order Fe-UZM-35(OP)0.38  $\approx$  Fe-UZM-35(OP)0.13 < Fe-UZM-35(OP)0.23. It is interesting to note that fresh Fe-UZM-35(OP)0.23 exhibits significantly higher in low-temperature  $\text{NH}_3$ -SCR activity than fresh Fe-beta(C)0.21, although the low-temperature activity becomes comparable after hydrothermal aging at 750 °C [11].

When differences in the framework Si/Al ratio of zeolite supports are not so large, in general, the standard SCR activity of Fe-exchanged zeolites are known to be less sensitive to the Fe loading level (or the Fe/Al ratio) than that of Cu-exchanged ones [28,29]. On the other hand, the conditions (170 °C, autogenic pressure, and air atmosphere) during the one-pot synthesis of Fe-UZM-35 would be considerably different from

those (80 °C, atmospheric pressure, and  $\text{N}_2$  atmosphere) during iron exchange in  $\text{NH}_4$ -UZM-35. It is then not difficult to expect that the state or intrazeolitic location of iron species in Fe-UZM-35(OP) could also be different from those in Fe-UZM-35(C). This may in our view be the major reason for the strong dependence of the SCR activity of Fe-UZM-35(OP) catalysts on their Fe/Al ratio. As shown in Fig. 4, however, the activity of Fe-UZM-35(OP)0.23 in both fresh and 750 °C-aged forms is essentially identical to that of Fe-UZM-35(C)0.24. The same result was also observed for the SCR activities of Cu-UZM-35(C)0.11 and Cu-UZM-35(OP)0.11 (Supplementary Fig. S5). Therefore, it is clear that Fe-UZM-35 with a high low-temperature activity can be conveniently and reproducibly one-pot synthesized, without careful iron exchange under inert  $\text{N}_2$  atmosphere. We also note that the amount of  $\text{N}_2\text{O}$  formed during  $\text{NH}_3$ -SCR over Fe-UZM-35(OP) catalysts under the conditions employed here is negligible (Supplementary Fig. S6), like the case for Fe-UZM-35(C) [21].



**Fig. 5.** Arrhenius plots for  $\text{NH}_3$ -SCR over the fresh and 750 °C-aged forms of (a) Fe-UZM-35(C)0.23 and (b) Fe-UZM-35(OP)0.24. Reaction conditions are the same as those in Fig. 4.

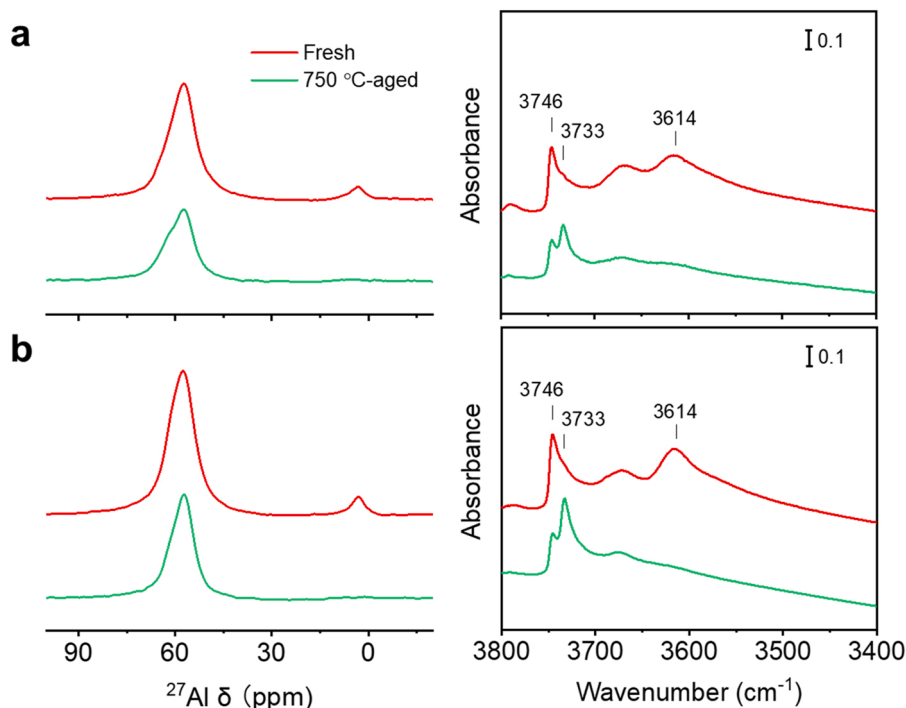


Fig. 6.  $^{27}\text{Al}$  MAS NMR (left) and IR (right) spectra in the OH region of the fresh and 750 °C-aged forms of (a) Fe-UZM-35(C)0.23 and (b) Fe-UZM-35(OP)0.24.

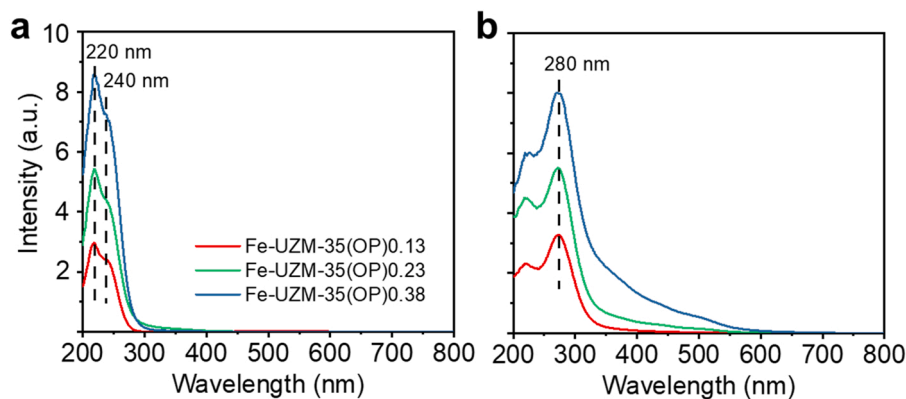


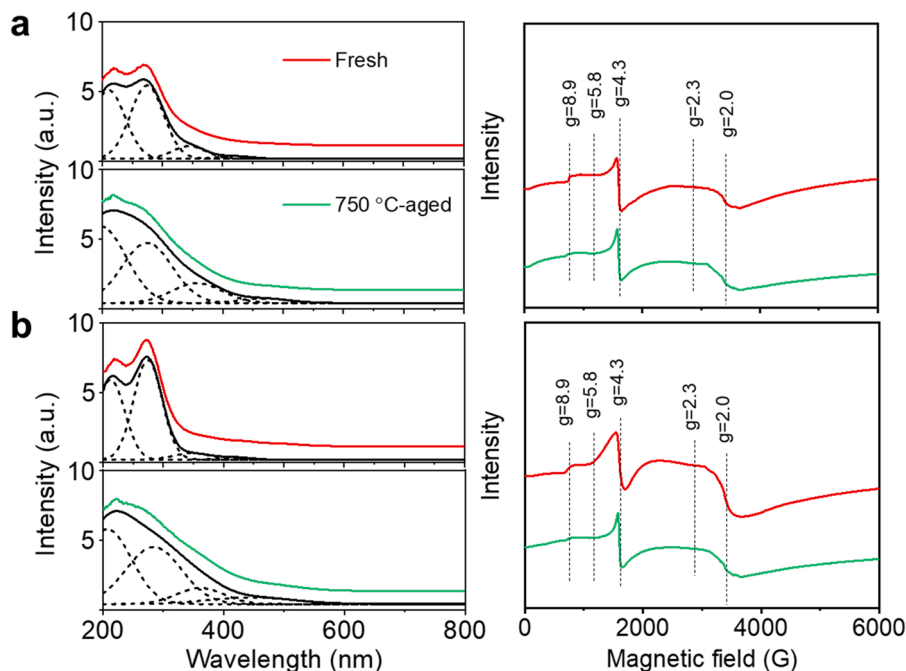
Fig. 7. UV-Vis spectra of the (a) as-made and (b) 550 °C-calcined forms of Fe-UZM-35(OP)0.13, Fe-UZM-35(OP)0.23, and Fe-UZM-35(OP)0.38.

### 3.3. Characterization

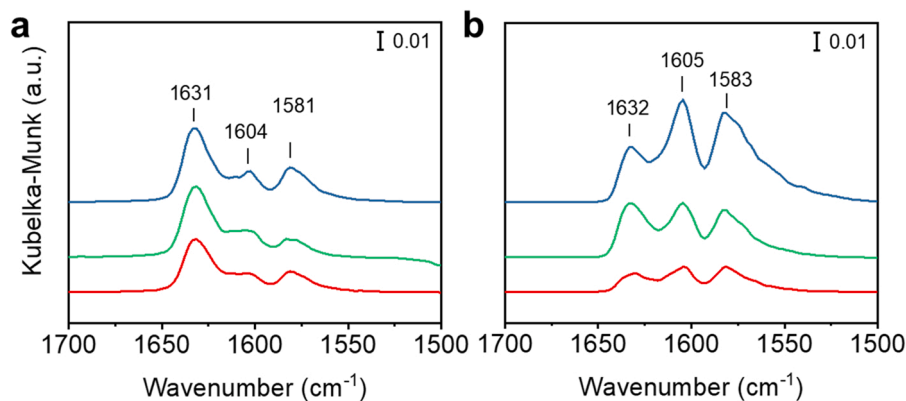
Fig. 5 shows the Arrhenius plots of Fe-UZM-35(C)0.24 and Fe-UZM-35(OP)0.23 for standard  $\text{NH}_3$ -SCR. No noticeable differences (52–56  $\text{kJ mol}^{-1}$ ) in the  $E_{\text{app}}$  value were observed for their fresh form, but also their 750 °C-aged one. This does not allow the active sites in the former catalyst to be distinguished from those in the latter one, again showing the merit of the one-pot synthesis of Fe-UZM-35. The PXRD patterns of three 750 °C-aged Fe-UZM-35(OP) catalysts with Fe/Al = 0.13–0.38 gave reflections from the MSE structure only (Supplementary Fig. S1). It thus appears that the formation of large iron oxide particles on the external surface of the zeolite crystals during hydrothermal aging at 750 °C may not be significant. The  $^{27}\text{Al}$  MAS NMR spectra of the fresh and 750 °C-aged forms of Fe-UZM-35(C)0.24 and Fe-UZM-35(OP)0.23 are compared in Fig. 6. An additional weak  $^{27}\text{Al}$  signal around 0 ppm is observed for the fresh form of both catalysts. Moreover, the tetrahedral  $^{27}\text{Al}$  signal resonance is considerably weaker for their 750 °C-aged form, because of severe dealumination during hydrothermal aging. This can be further supported by their IR spectra in the OH region. As shown in Fig. 6, the OH band appearing at 3614  $\text{cm}^{-1}$  due to

Si-OH-Al Brønsted acid sites [11] is hardly observable for 750 °C-aged Fe-UZM-35(C)0.24 and Fe-UZM-35(OP)0.23 both, which matches well with a notable intensity increase of the IR band at 3733  $\text{cm}^{-1}$ , assignable to internal Si-OH groups [30,31]. It is also remarkable that the acidic properties of the fresh and 750 °C-aged forms of Fe-UZM-35(OP)0.23 have a strong resemblance to those of the corresponding forms of Fe-UZM-35(C)0.24, respectively, because the  $\text{NH}_3$  TPD profiles of these two pair of Fe-UZM-35 catalysts are characterized by similar line shapes and areas (Supplementary Fig. S7).

Fig. 7 shows the UV-Vis spectra of the as-made and 550 °C-calcined forms of three Fe-UZM-35(OP) zeolites with different Fe/Al ratios (0.13–0.38) in the hydrated state. The spectra of all as-made zeolites have almost the same line shape so that two  $\text{Fe}^{3+} \leftarrow \text{O}$  charge-transfer (CT) bands around 220 and 240 nm, attributable to the isolated framework  $\text{Fe}^{3+}$  ions [32], can be resolved, with nearly constant relative intensities. In fact, we cannot exclude the possibility that partial Fe substitution has occurred during UZM-35(OP) synthesis, because no specific iron chelating agents were intentionally added to the synthesis mixture. As shown in Fig. 7, on the other hand, calcination of as-made Fe-UZM-35(OP) zeolites at 550 °C results in the appearance of a new



**Fig. 8.** UV-Vis (left) and EPR (right) spectra of the fresh and 750 °C-aged forms of (a) Fe-UZM-35(C)0.23 and (b) Fe-UZM-35(OP)0.24. The EPR spectra were collected at  $-148$  °C.



**Fig. 9.** DRIFT spectra of NO adsorbed on fresh (a) Fe-UZM-35(C)0.14, Fe-UZM-35(C)0.24, and Fe-UZM-35(C)0.35 (bottom to top) and (b) Fe-UZM-35(OP)0.13, Fe-UZM-35(OP)0.23, and Fe-UZM-35(OP)0.38 (bottom to top). All the spectra were recorded at 150 °C after exposure to the feed gas containing 500 ppm NO and 5%  $\text{O}_2$  in He flow for 1 h followed by purging in a He flow at the same temperature for another 0.5 h.

strong band around 280 nm. This implies that well-dispersed extra-framework  $\text{Fe}^{3+}$  ions in octahedral coordination may be one of the major iron species in calcined Fe-UZM-35(OP) zeolites [18].

Fig. 8 shows the UV-Vis spectra of the fresh and 750 °C-aged forms of Fe-UZM-35(C)0.24 and Fe-UZM-35(OP)0.23 in the hydrated state. The spectra of both fresh catalysts exhibit two CT bands around 220 and 280 nm, together with two weaker CT bands around 350 and 450 nm that can be attributed to small  $\text{Fe}_x\text{O}_y$  clusters and larger  $\text{Fe}_2\text{O}_3$  particles, respectively [33,34]. While the band around 280 nm becomes weaker after hydrothermal aging at 750 °C, the opposite holds for the two bands around 220 and 280 nm. Deconvolution of the UV-Vis spectra in Fig. 8 reveals that the relative intensity distribution of these four CT bands is nearly the same for the two pairs of Fe-UZM-35 catalysts (Supplementary Table S1). Also, hydrothermal aging at 750 °C led to no decrease in relative intensity for the band around 220 nm ascribed to tetrahedral  $\text{Fe}^{3+}$  ions. The same result was found in the UV-Vis spectra (not shown) of two pairs of Fe-UZM-35(C) and Fe-UZM-35(OP) zeolites with lower (ca. 0.13) and higher (ca. 0.36) Fe/Al ratios. Therefore, the octahedral

extra-framework  $\text{Fe}^{3+}$  ions appear to be more responsible for the high low-temperature ( $<350$  °C) SCR activity of fresh Fe-UZM-35, because water is among the key components in vehicle exhaust. The X-band EPR spectra at  $-148$  °C of the above four catalysts are also compared in Fig. 8. No noticeable changes in the EPR line shape by hydrothermal aging were observed, except some intensity decrease of the two low-field signals at g values of 8.9 and 5.8, probably owing to the partial transformation of isolated  $\text{Fe}^{3+}$  species to iron oxide species [35,36].

Fig. 9 shows the DRIFT spectra of adsorbed NO on three pairs of fresh Fe-UZM-35(C) and Fe-UZM-35(OP) catalysts with different Fe/Al ratios. All the spectra are characterized by three bands at 1632, 1605, and 1583  $\text{cm}^{-1}$ . The first band at 1632  $\text{cm}^{-1}$  is assigned to  $\text{Fe}^{3+}$  mononitrosyl species, whereas the other two bands at 1605 and 1583  $\text{cm}^{-1}$  reflect the formation of  $\text{Fe}^{3+}$  nitrate species, respectively [37–39]. No dependence of the relative intensity on Fe/Al ratio was observed for these three bands from fresh Fe-UZM-35(C) catalysts. As shown in Fig. 9, however, this is not the case for Fe-UZM-35(OP) ones. For example, the two bands at 1605 and 1583  $\text{cm}^{-1}$  become stronger with increasing

Fe/Al ratio from 0.13 to 0.38. Also, the relative intensity of the band at  $1632\text{ cm}^{-1}$  is significantly weaker from Fe-UZM-35(OP)0.13 than from Fe-UZM-35(C)0.14, despite essentially the same Fe/Al ratio (ca. 0.13). Recall that the low-temperature activity of the former catalyst is considerably poorer than that of the latter one (Fig. 4). We speculate that this can be attributed to differences in the intrazeolitic location of their isolated  $\text{Fe}^{3+}$  ions, which deserves further study.

Finally, we have also carried out UV-vis and Cu K-edge XANES measurements on the fresh and  $750^\circ\text{C}$ -aged forms of Cu-UZM-35(C)0.10 and Cu-UZM-35(OP)0.11 catalysts. No noticeable differences in the type and distribution of various copper species in their respective Cu-UZM-35 catalysts were found (Supplementary Table S2 and Figs. S8 and S9), in line with their SCR activities (Supplementary Fig. S5).

#### 4. Conclusions

In summary, we have synthesized the large-pore zeolite UZM-35 by combining the IZC route with the seeding method, using USY zeolites as both Al and Si-sources in the presence of DMDPA as an OSDA. We were also successful in the one-pot-synthesis of Fe-UZM-35 which is much more convenient and reproducible than the post-synthetic preparation of iron-exchanged UZM-35, because there is no need for careful iron exchange under  $\text{N}_2$  atmosphere and repeated calcination steps. This route also allows Fe-UZM-35 crystallization to be complete within 1.5 days, which is considerably shorter than the crystallization time (7 days) of conventional UZM-35. The  $\text{NH}_3$ -SCR activities of one-pot-synthesized and post-synthetically exchanged Fe-UZM-35 zeolites with similar Fe/Al ratios (ca. 0.23) were found to be essentially identical to each other in the reaction temperature range studied, regardless of hydrothermal aging at  $750^\circ\text{C}$ . The overall characterization results show no notable differences in the nature of their iron active sites. However, the intrazeolitic location of isolated  $\text{Fe}^{3+}$  ions, known as active sites for low-temperature  $\text{NH}_3$ -SCR, could be different because of notable differences in the temperature, pressure, and atmosphere of the one-pot Fe-UZM-35 synthesis compared to iron exchange in  $\text{NH}_4$ -UZM-35. We expect that this study will provide useful insight into the facile synthesis of metal-loaded zeolites with interesting  $\text{NH}_3$ -SCR performance but poor synthesis reproducibility.

#### CCRediT authorship contribution statement

**Xuechao Tan:** Conceptualization, Methodology, Investigation, Writing – original draft. **Shoute Zhang:** Conceptualization, Methodology, Investigation, Writing – original draft. **Suk Bong Hong:** Conceptualization, Supervision, Writing – review & editing, Project administration, Funding acquisition.

#### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### Data Availability

Data will be made available on request.

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#### Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.apcatb.2023.122552.

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